

张耀平\*

710123

**Proposal of Auxiliary Pumping Technique Taking-in and Pushing-out  
Low-Pressure Air with Running Vehicle in Vacuum Tube Transport**

Zhang Yaoping\*

*Institute of Vacuum Tube Transport Xijing University Xi'an 710123 China*

2 5000 10000 km/h  
6  $1.101325 \times 10^0 \sim$   
 $1.101325 \times 10^{-1}$  Pa

" " 5  
3

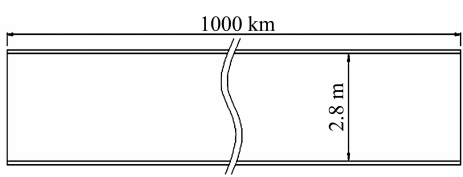
1.3 假设

1  
2 /  
3

1 分析模型、假设

1.1 管道模型

1 2.8 m  
1000 km



1

Fig.1 Schematic diagram of the tube structure in vacuum tube transport

1.2 抽真空阶段模型

1 ~ 1/10 1/10 ~ 1/100 1/100 ~ 1/1000 1/1000 ~ 1/10000 1/10000 ~ 1/100000 atm

1  $1.101325 \times 10^5 \sim 1.101325 \times 10^4$  Pa  
2  $1.101325 \times 10^4 \sim 1.101325 \times 10^3$  Pa  
3  $1.101325 \times 10^3 \sim 1.101325 \times 10^2$  Pa  
4  $1.101325 \times 10^2 \sim 1.101325 \times 10^1$  Pa  
5  $1.101325 \times 10^1 \sim 1.101325 \times 10^0$  Pa

5  
5

2 真空泵排气方式形成真空的功率与能耗

$V = 6154400 \text{ m}^3$   $6154.4 \text{ m}^3$   
1000 km

10 m  
1 ~ 10 km 2 ~ 5 km  
5 km

$S_e = 5 \text{ m}^3/\text{s}$

$p_0$   $p_1 = 1.01325 \times 10^2 \text{ Pa}$   
6

$t = \frac{V}{S_e} \ln \frac{p_0}{p_1} = \frac{5 \times 6154.4}{5} \ln \frac{1.01325 \times 10^5}{1.01325 \times 10^2}$   
 $= 6154.4 \times \ln 1000 = 2 \text{ s} = 11.8 \text{ h}$   
 $V$   $R_1$

5  $\text{m}^3/\text{s}$   
200 kW 5 km 1000 km  
200  
40000 kW 11.8 h  
472000 kWh  
1/10  $p_1 = 10132.5$   
Pa

$$t = \frac{5 \times 6154.4}{5} \ln \frac{101325}{10132.5} = 6154.4 \times \ln 10$$

$$= 14171 \text{ s} = 3.94 \text{ h}$$

157600 kWh

$$p_2 \quad V_2$$

$$p_0 V_{vp0} = p_2 V_2 \quad 4$$

$$V_2 = \frac{p_0 V_{vp0}}{p_2} \quad 5$$

$$V_2 = V \frac{p_0 - p_1}{p_2} \quad 6$$

$$1/1000 \quad p_1 =$$

$$101.325 \text{ Pa} \quad p_2 = 15 \text{ MPa}$$

6

$$V_2 = 6154400 \times \frac{101325 - 101.325}{15 \times 10^6} = 41531 \text{ m}^3$$

$$101.325 \quad 10.1325 \quad 1.01325 \text{ Pa} \quad 10132.5 \quad 1013.25$$

$$10 \quad 15 \quad 20 \quad 25 \quad 30 \quad 35 \quad 40 \text{ MPa} \quad p_2$$

1

### 3 车辆运行抽气方式形成真空的功率与能耗

#### 3.1 所需储气瓶容积总和计算

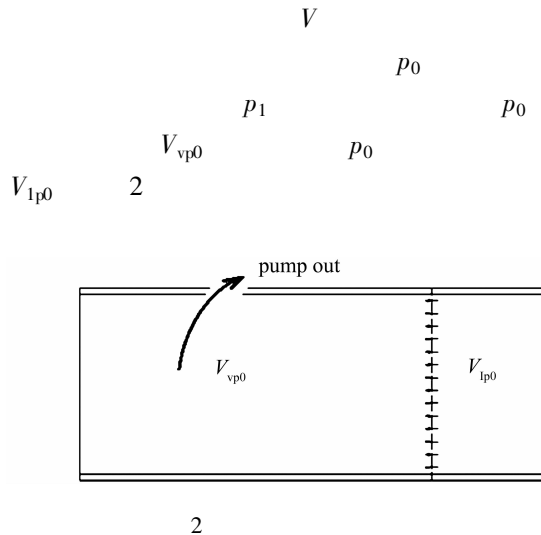


Fig.2 Schematic illustration of the variations in gas volume

$$V_{vp0} + V_{lp0} = V \quad 1$$

$$\frac{p_1}{p_0} = \frac{V_{lp0}}{V} = \frac{V - V_{vp0}}{V} \quad 2$$

$$V_{vp0} = V \left( 1 - \frac{p_1}{p_0} \right) \quad 3$$

表 1 所需要的储气容器总容积

Tab.1 Required total capacity of the gas storage tanks

$p_1/\text{Pa}$	/m <sup>3</sup>						
	10	15	20	25	30	35	40
10132.5	56124	37416	28062	22449	18708	16035	14031
1013.25	61736	41157	30868	24694	20579	17639	15434
101.325	62297	41531	31149	24919	20766	17799	15574
10.1325	62353	41569	31177	24941	20784	17815	15588
1.01325	62359	41573	31179	24944	20786	17817	15590

2.8 m

1 ~ 2.4 m

0.785 ~

4.5216 m<sup>2</sup>

10 m

7.8 ~ 45.216 m<sup>3</sup>

2

表 2 所需不同压力级储气瓶数

Tab.2 Required number of the high pressure gas storage tank

$p_1/\text{Pa}$							
	10	15	20	25	30	35	40
10132.5	7150/1241	4766/828	3575/621	2860/497	2383/414	2043/355	1787/310
1013.25	7864/1365	5243/910	3932/683	3146/546	2622/455	2247/390	1966/341
101.325	7936/1378	5290/919	3968/689	3174/551	2645/459	2267/394	1984/344
10.1325	7943/1379	5295/919	3972/690	3177/552	2648/460	2270/394	1986/345
1.01325	7944/1379	5296/919	3972/690	3178/552	2648/460	2270/394	1986/345

注:

1 m

2.4 m

2  $p_2 = 40 \text{ MPa}$  1/10 1/100  
 2.4 m 10 m  
 1/1000 344  
 1000 km 100  
 3.5  
 $V_{vp0} = V \left(1 - \frac{1013.25}{101325}\right) - 5538960$   
 $= 6154400 \times (1 - 0.01) - 5538960$   
 $= 553896 \text{ m}^3$   
 1/10 1/10  
 3

3.2 排出气体量计算

3 1/10 3 3 2  
 $V_{vp0} = V \left(1 - \frac{p_1}{p_0}\right) = 6154400 \times (1 - 0.1) = 5538960 \text{ m}^3$   
 1/10 5 1/10000  
 1/100000 1  
 1/10 1/  
 90% 10000

表 3 各阶段排气量及所占总量的百分比

Tab.3 Percentage of the gas pumped out in each stage

	1	2	3	4	5
/1.101325 Pa	$10^5 \rightarrow 10^4$	$10^4 \rightarrow 10^3$	$10^3 \rightarrow 10^2$	$10^2 \rightarrow 10^1$	$10^1 \rightarrow 10^0$
/m <sup>3</sup>	5538960	553896	55389.6	5538.96	553.896
/%	90	9	0.9	0.09	0.009

3.3 运行排气方式形成真空功耗计算

100 m<sup>3</sup>/min 10 ~ 1  
 100 MPa 250  
 kW 1000 kWh  
 1/10 2  
 5538960 m<sup>3</sup> 1  
 55390 min 923 h 2  
 923 h  
 1 1/10  
 2 1 1/10  
 46150 kWh 3 4615  
 250 kW kWh 4 5 461.5  
 1000 kWh 46.15 kWh  
 1/10 923 × 500 1000  
 = 461500 kWh 923 × 2000 = 1846000 kWh kW 2  
 500 kW 2  
 1 1/10 92.3 × 1500 = 138450 kWh

### 4 真空泵站与运行抽气相结合的抽真空方式

	1/1000		$p_1 = 101.325 \text{ Pa}$		1/1000		1/100	
	11.8 h		1/10					
$p_0$			3.94 h					
	1/10	/	1/1000					
	/	1/3					5 km	$S_e = 5$
			1/	$\text{m}^3/\text{s}$	1013.25 Pa	102.325 Pa		
10	1		90%		3.94 h	157600 kWh		
					3	2.8 m	1000 km	
	1				1013.25 Pa	102.325 Pa		
	2		1/10					
	$\Phi 2.4 \times 10 \text{ m}$	*	40 MPa		$V_{vp0} = V_i \left(1 - \frac{101.325}{101325}\right) - V_i \left(1 - \frac{1013.25}{101325}\right)$			
310	$\Phi 1 \times 10 \text{ m}$		15 MPa		$= 615440 \times 0.01 - 0.001$			
					$= 609286 \times 0.009$			
	4766				$= 5484 \text{ m}^3$			
	2				6	15 MPa		
		100 $\text{m}^3/\text{min}$	10 ~					
100 MPa								
	1/10		5538960 $\text{m}^3$					
	55390 min							
		1/10						
100	$\Phi 2.4 \times 10 \text{ m}$		40 MPa	1/				
	$\Phi 1 \times 10 \text{ m}$		15 MPa	477		100 $\text{m}^3/\text{min}$		10 ~
	5539 min							1/100
		1/10		1/100	1/1000		54.84 min	
			1/10					1000
	1/10				9		1/100	
					km/h		150 kN	
1/10								
	1							
							2000 kW	
	2		1/10		250 kW			200
	1/100		1/10		km/h		5 h	
			/		11250 kWh			
							1000 Pa	
							1000 km	200

### 5 恢复真空补抽气时的功率消耗

+ 40  $\text{m}^3$  15 MPa  
+ "

### 7 结论

#### 6 上述估算分析的可信度

##### 6.1 能耗估算结果可信度及其对研究结论的影响

1			1	1/10	90%	1
2	2.8 m	5 km	2			
		6-8 11				
3	5 m <sup>3</sup> /s	200				1
kW			3	1		
4		250 kW				
			4	1/10		1/100
			2			
			10%			
		157600 × 3 = 472800 > 461500 kWh				
1						
	2					

##### 6.2 建设成本估算结果可信度及其对研究结论的影响

			5	1/100		1/1000
			3			
			1%			
					4	5
	1		6			
			2			
	2		①			
1					②	1
						2
2						
			③			

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